

## The liquid Cd–Ga–Sn: enthalpy of formation

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### Abstract

Using a high temperature calorimeter, the enthalpy of formation of the liquid ternary Cd–Ga–Sn system has been determined at 740 K. The enthalpy of formation is positive over the entire concentration range and can be represented by the following modified Muggianu's relation:

$$\begin{aligned}\Delta_{\text{mix}}H_m = & \frac{4x_Bx_C}{(2x_B+x_C)(2x_C+x_A)} [\Delta_{\text{mix}}H_{m(\text{BC})}]_{x_B(\text{BC})=x_B+x_A/2} \\ & + \frac{4x_Ax_C}{(2x_A+x_B)(2x_C+x_B)} [\Delta_{\text{mix}}H_{m(\text{AC})}]_{x_A(\text{AC})=x_A+x_B/2} \\ & + \frac{4x_Ax_B}{(2x_A+x_C)(2x_B+x_C)} [\Delta_{\text{mix}}H_{m(\text{AB})}]_{x_A(\text{AB})=x_A+x_C/2} + x_Ax_Bx_C(ax_A + bx_B + cx_C)\end{aligned}$$

where  $x_A$  and  $x_{A(\text{AB})}$  are the molar fractions of A in the ternary A–B–C and binary A–B alloys respectively,  $x_A = x_{\text{Cd}}$ ,  $x_B = x_{\text{Ga}}$ ,  $x_C = x_{\text{Sn}}$ ,  $a = -4.50(8)$  kJ mol<sup>-1</sup>,  $b = +11.67(9)$  kJ mol<sup>-1</sup>,  $c = -4.59(3)$  kJ mol<sup>-1</sup> and using the binary data already published.

### 1. Introduction

In the course of a systematic thermodynamic investigation of alloys exhibiting a liquid miscibility gap, thermodynamic measurements have been performed on the Cd–Ga–Sn system. In the same way as for the Al–Bi–Ga system, the aim of this work is (i) to determine the localization of the miscibility gap using several techniques (calorimetry, differential thermal analysis,  $C_p = f(T)$  measurements etc.) and (ii) to make a comparison between experimental and calculated equilibrium temperatures [1]. Moreover the influence of the addition of the third metal (here tin) on the miscibility gap will be studied.

According to available compilations [2, 3], the equilibrium phase diagram, enthalpy and free energy of formation of the Cd–Ga–Sn system are unknown. In the present paper the heat of mixing data will be reported and a relation will be proposed for the enthalpy of formation of the Cd–Ga–Sn liquid alloy over the entire concentration range.

## 2. Bibliographic survey

For the limiting binary systems, the main information concerning the phase diagram and the enthalpy of formation are reported in the following section. These data are essential to choose the best experimental procedure and to predict ternary enthalpy data.

### 2.1. Cd–Ga system

#### 2.1.1. Phase diagram

A small miscibility gap has been found. According to Heumann *et al.* [4] and Atamanova *et al.* [5], the coordinates of monotectic and critical points are  $T_m = 555$  K with  $x_{Ga} = 0.227$  and  $T_c = 568$  K with  $x_{Ga} = 0.506$  respectively. The conjugate point of the monotectic is at  $x_{Ga} = 0.725$ . The eutectic temperature is very close to the melting point of pure gallium ( $T_e = 302.53$  K at  $x_{Ga} = 0.99$ ). The solid solubility of cadmium in gallium is negligible; that of gallium in cadmium is less than 1 at.%. All these data were obtained by Moser and co-workers [6].

#### 2.1.2. Enthalpy of mixing

The enthalpy of formation of liquid Cd–Ga alloys, using direct calorimetry, was determined by Kleppa [7] at 623 K for the molar fraction range  $0.02 < x_{Ga} < 0.89$  and by Moser *et al.* [8] between 602 and 696 K for the molar fraction range  $0.014 < x_{Cd} < 0.97$ . A temperature dependence has been noticed; the mean value of  $\Delta C_p$  between 609 and 695 K is about  $5.7 \text{ J K}^{-1} \text{ mol}^{-1}$ . In 1981, Vecher *et al.* [9] published new results on the enthalpies of formation of Cd–Ga and Cd–Ga–In liquid alloys at 630 K. Their values of binary enthalpies, which were very similar to Kleppa's results (a difference of about  $60 \text{ J mol}^{-1}$  at  $x_{Cd} = 0.5$ ) have been used for this study:

$$\begin{aligned} \Delta_{\text{mix}} H_{m(\text{Cd}+\text{Ga})(l)} &= x_{Ga}(1-x_{Ga})(15.0(39) - 17.4(91)x_{Ga}) \\ &= 16.4(05)x_{Ga}^2 - 0.02_1 x_{Ga}^3 \text{ kJ mol}^{-1} \end{aligned} \quad (1)$$

and the values of the limiting molar partial enthalpies are respectively

$$\Delta H_{m^\circ \text{ Ga}(l) \text{ in Cd}(l)} = +13.9(3) \text{ kJ mol}^{-1}$$

$$\Delta H_{m^\circ \text{ Cd}(l) \text{ in Ga}(l)} = +15.0(4) \text{ kJ mol}^{-1}$$

### 2.2. Cd–Sn system

#### 2.2.1. Phase diagram

The liquidus temperatures obtained by several workers are in good agreement. The Cd–Sn phase diagram shows a eutectic point ( $x_{Sn} = 0.6655$  at  $T = 449$  K) and an intermediate solid phase ( $\beta$ ) of simple hexagonal A3 structure. The coordinates of the peritectic and eutectic points found by various researchers differ significantly and are close to  $T = 496$  K with  $x_{Sn} = 0.99$  and  $T = 406$  K with  $x_{Sn} = 0.947$ . The maximum solubility of tin in cadmium is  $x_{Sn} = 0.0024$  at 449 K. Dutkiewicz *et al.* [10] have used  $x_{Cd} = 0.0063$  at 496 K for the solubility of cadmium in tin.

### 2.2.2. Enthalpy of mixing

The following equation was obtained from the results compiled by Hultgren *et al.* [11] and obtained by Kleppa [12] using direct calorimetry between 623 and 723 K and by Elliott [13] at 773 K using potentiometric measurements (these two sets of data are in good agreement; calorimetric data previously published by Kawakami [14] are lower than those of Kleppa):

$$\Delta_{\text{mix}} H_{\text{m}(\text{Cd}+\text{Sn})} = x_{\text{Sn}}(1-x_{\text{Sn}})(9.8(62) - 7.5(27)x_{\text{Sn}} + 4.4(35)x_{\text{Sn}}^2 + 0.02(4)x_{\text{Sn}}^3) \text{ kJ mol}^{-1} \quad (2)$$

with the following limiting molar partial enthalpies:

$$\Delta H_{\text{m}^{\circ} \text{Cd(l)} \text{ in Sn(l)}} = +6.7(9) \text{ kJ mol}^{-1}$$

$$\Delta H_{\text{m}^{\circ} \text{Sn(l)} \text{ in Cd(l)}} = +9.8(6) \text{ kJ mol}^{-1}$$

By means of isoperibolic solution calorimetry, Boom [15] found  $\Delta H_{\text{m}^{\circ} \text{Cd(l)} \text{ in Sn(l)}} = +7.28 \pm 0.11 \text{ kJ mol}^{-1}$ .

### 2.3. Ga-Sn system

#### 2.3.1. Phase diagram

The liquidus exhibits a eutectic point near pure gallium ( $T_{\text{E}} = 293.6 \text{ K}$  at  $x_{\text{Ga}} = 0.915$ ) [16]. At the eutectic temperature, the solid solubilities are as follows: in gallium,  $x_{\text{Sn}} = 0.017$  [17] and, in tin,  $x_{\text{Ga}} = 0.071$  [16].

#### 2.3.2. Enthalpy of mixing

Between 400 and 700 K, the heat of formation of liquid Ga-Sn alloys was measured by direct calorimetry by Predel [18] and Bros *et al.* [19]. The enthalpy of mixing, which is positive and not temperature dependent, can be represented by

$$\Delta_{\text{mix}} H_{\text{m}(\text{Ga}+\text{Sn})} = x_{\text{Sn}}(1-x_{\text{Sn}})(3.80(5) - 0.82(4)x_{\text{Sn}} + 0.29(8)x_{\text{Sn}}^2 - 0.009x_{\text{Sn}}^3) \text{ kJ mol}^{-1} \quad (3)$$

and the values of the limiting partial enthalpies are

$$\Delta H_{\text{m}^{\circ} \text{Ga(l)} \text{ in Sn(l)}} = +3.2(8) \text{ kJ mol}^{-1}$$

$$\Delta H_{\text{m}^{\circ} \text{Sn(l)} \text{ in Ga(l)}} = +3.8(1) \text{ kJ mol}^{-1}$$

Boom's [15] value is  $\Delta H_{\text{m}^{\circ} \text{Ga(l)} \text{ in Sn(l)}} = +2.82 \text{ kJ mol}^{-1}$  at 600 K.

Figure 1 shows the three limiting phase diagrams and the six sections along which the calorimetric experiments were performed.

## 3. Experimental procedure

High purity (99.999 at.%) metals were employed in this study. Cadmium and tin were rinsed with acetone p.a., dried and cut in small pieces. The

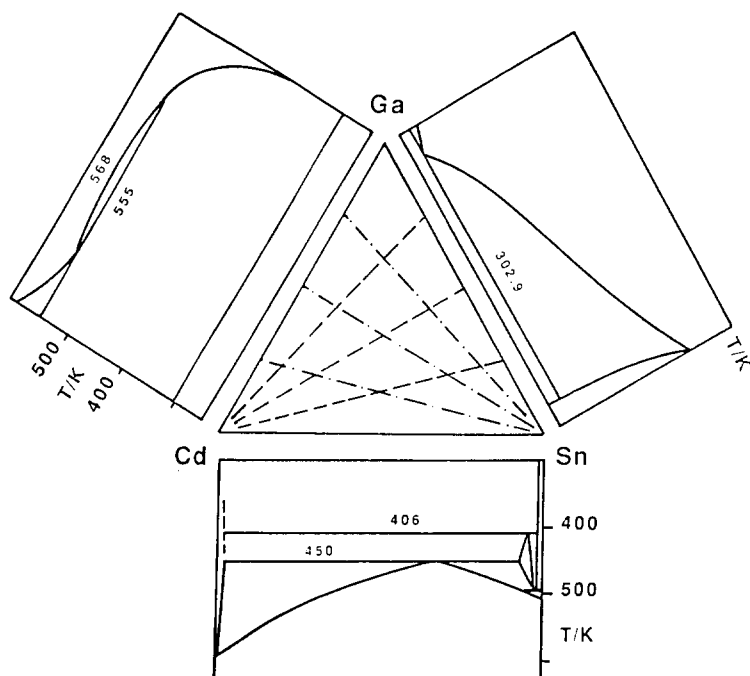


Fig. 1. The limiting binary systems and the six sections along which the calorimetric experiments were performed at 740 K.

gallium was melted in a warm (35 °C) dilute solution of hydrochloric acid (5%) in water, separated in small droplets and dried after rinsing with cold water.

A Calvet high temperature calorimeter, equipped with an automatized sample charger was employed. The experiments were carried out in high purity argon. Argon U (Air Liquid Company) was further purified by passing over a titanium sponge (1100 K) to get the remaining oxygen. Calibration was accomplished by dropping small pieces of  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> (samples from National Institute of Standards and Technology) from room temperature into the experimental crucible at the end of each measurements series.

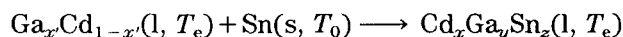
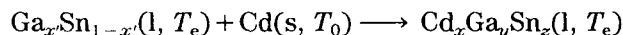
The alloys were formed by multiple successive additions of cadmium (or tin) to the liquid Ga-Sn (or Ga-Cd) liquid bath contained in a graphite crucible of about 50 mm height and 8 mm inside diameter. This graphite crucible is located in the gas-tight silica cell. A complete description of this device has been published previously [20].

The standard deviation of the enthalpies were found to be about 20 or 40 J mol<sup>-1</sup> for two independent series at the same binary molar fraction. Errors were estimated to be of the same order of magnitude (2–3%) as the difference found for the calibration drops. However, if we take into account the uncertainty in the enthalpy of formation of the limiting alloys, the final accuracy of the enthalpy of formation of Cd-Ga-Sn is about  $\pm 4\%$ . The

experimental temperature ( $740 \pm 1$  K) was determined with a Pt-(Pt-10wt.% Rh) thermocouple.

#### 4. Results and discussion

To obtain the enthalpy of formation of the Cd-Ga-Sn liquid alloys (at  $T_e$ ), two types of experiment were performed either by additions (at  $T_0$  (room temperature)) of solid cadmium or of solid tin corresponding to



$T_e = 740$  K and  $x'$  and  $x$ ,  $y$ ,  $z$  are the binary and ternary molar fractions respectively.

$$x_{\text{Ga}}/x_{\text{Sn}} = 1/3 \text{ with } 0 < x_{\text{Cd}} < 0.51$$

$$x_{\text{Ga}}/x_{\text{Sn}} = 1/1 \text{ with } 0 < x_{\text{Cd}} < 0.60$$

$$x_{\text{Ga}}/x_{\text{Sn}} = 3/1 \text{ with } 0 < x_{\text{Cd}} < 0.60$$

and

$$x_{\text{Cd}}/x_{\text{Ga}} = 1/3 \text{ with } 0 < x_{\text{Sn}} < 0.62$$

$$x_{\text{Cd}}/x_{\text{Ga}} = 1/1 \text{ with } 0 < x_{\text{Sn}} < 0.58$$

$$x_{\text{Cd}}/x_{\text{Ga}} = 3/1 \text{ with } 0 < x_{\text{Sn}} < 0.58$$

Along each quasi-binary section, at least two experiments have been performed.

The resulting integral enthalpies are collected in Tables 1 and 2. The values of the molar heat capacity and enthalpy of the melting of tin and cadmium published by Hultgren *et al.* [21] were used to transform our results to the liquid state.

Table 3 in which the enthalpies of formation at the intersection points A, ..., I are given allow us to criticize the reproducibility of these experiments. As we can see, for the same ternary alloy the discrepancy between the enthalpy obtained by dropping cadmium or tin is less than 4%.

Moreover, from the calorimetric results, the limiting molar partial enthalpies of dissolution of cadmium and tin have been deduced (Table 4). Obviously, these data obtained by interpolation of our experimental results are less precise than integral molar enthalpies (about 10%). Nevertheless we can note that the enthalpies of dissolution of tin (or cadmium) in Ga-liquid alloys with increasing molar fraction of cadmium (or tin) change very regularly (Table 4).

To predict the enthalpy of formation, we have used the geometric considerations proposed by Kohler [22] and Muggianu *et al.* [23] and a model developed by Hoch and Arpshofen [24] and Hoch [25].

The relations proposed by Kohler and Muggianu *et al.* are:

TABLE 1

Experimental values of the enthalpy of formation of the Cd–Ga–Sn liquid alloys (at 740 K) obtained by additions of cadmium to liquid binary Ga–Sn alloys ( $x_{\text{Ga}}/x_{\text{Sn}} = 1/3, 1/1$  and  $3/1$ ) and referred to the liquid state

| $x_{\text{Ga}}/x_{\text{Sn}} = 1/3$ |   | $x_{\text{Ga}}/x_{\text{Sn}} = 1/1$ |   | $x_{\text{Ga}}/x_{\text{Sn}} = 3/1$ |   |
|-------------------------------------|---|-------------------------------------|---|-------------------------------------|---|
| $x_{\text{Cd}}$                     | $\Delta_{\text{mix}}H_{\text{m}}$<br>(J mol <sup>-1</sup> ) | $x_{\text{Cd}}$                     | $\Delta_{\text{mix}}H_{\text{m}}$<br>(J mol <sup>-1</sup> ) | $x_{\text{Cd}}$                     | $\Delta_{\text{mix}}H_{\text{m}}$<br>(J mol <sup>-1</sup> ) |
| 0.0000                              | 629   | 0.0000                              | 867   | 0.0000                              | 678   |
| 0.0330                              | 796   | 0.0427                              | 1198  | 0.0520                              | 1100  |
| 0.0344                              | 813   | 0.0711                              | 1332  | 0.0561                              | 1233  |
| 0.0867                              | 1098  | 0.0904                              | 1450  | 0.1074                              | 1561  |
| 0.0916                              | 1125  | 0.0934                              | 1557  | 0.1168                              | 1678  |
| 0.1372                              | 1347  | 0.1419                              | 1701  | 0.1368                              | 1746  |
| 0.1966                              | 1621  | 0.1512                              | 1746  | 0.1977                              | 2040  |
| 0.2435                              | 1774  | 0.2012                              | 1874  | 0.2060                              | 2184  |
| 0.2484                              | 1742  | 0.2058                              | 2081  | 0.2230                              | 2174  |
| 0.2938                              | 1864  | 0.2104                              | 2008  | 0.2645                              | 2337  |
| 0.3074                              | 1963  | 0.2517                              | 2151  | 0.2764                              | 2395  |
| 0.3280                              | 1938  | 0.2593                              | 2198  | 0.3200                              | 2560  |
| 0.3570                              | 1999  | 0.2872                              | 2283  | 0.3369                              | 2595  |
| 0.3680                              | 2094  | 0.2964                              | 2428  | 0.3455                              | 2597  |
| 0.3842                              | 2062  | 0.3091                              | 2315  | 0.3704                              | 2730  |
| 0.4115                              | 2128  | 0.3095                              | 2421  | 0.3895                              | 2705  |
| 0.4196                              | 2101  | 0.3480                              | 2530  | 0.4147                              | 2743  |
| 0.4625                              | 2176  | 0.3809                              | 2485  | 0.4244                              | 2775  |
| 0.5043                              | 2182  | 0.3845                              | 2537  | 0.4397                              | 2805  |
| 1.0000                              | 0   | 0.3882                              | 2584  | 0.4817                              | 2802  |
|                                     |   | 0.4447                              | 2546  | 0.5263                              | 2778  |
|                                     |   | 0.4457                              | 2618  | 0.5642                              | 2739  |
|                                     |   | 0.4984                              | 2559  | 0.5979                              | 2700  |
|                                     |   | 0.5032                              | 2642  | 1.0000                              | 0   |
|                                     |   | 0.5438                              | 2655  |                                     |   |
|                                     |   | 0.5975                              | 2576  |                                     |   |
|                                     |   | 1.0000                              | 0   |                                     |   |

$$\Delta_{\text{mix}}H_{\text{m}} = (x_{\text{A}} + x_{\text{B}})^2 [\Delta_{\text{mix}}H_{\text{m}(\text{AB})}] x_{\text{A}}/x_{\text{B}}$$

$$+ (x_{\text{A}} + x_{\text{C}})^2 [\Delta_{\text{mix}}H_{\text{m}(\text{AC})}] \frac{x_{\text{A}}}{x_{\text{C}}} + (x_{\text{B}} + x_{\text{C}})^2 [\Delta_{\text{mix}}H_{\text{m}(\text{BC})}] x_{\text{B}}/x_{\text{C}}$$

$$\Delta_{\text{mix}}H_{\text{m}} = \frac{4x_{\text{B}}x_{\text{C}}}{(2x_{\text{B}} + x_{\text{A}})(2x_{\text{C}} + x_{\text{A}})} [\Delta_{\text{mix}}H_{\text{m}(\text{BC})}]_{x_{\text{B}(\text{BC})} = x_{\text{B}} + x_{\text{A}}/2}$$

$$+ \frac{4x_{\text{A}}x_{\text{C}}}{(2x_{\text{A}} + x_{\text{B}})(2x_{\text{C}} + x_{\text{B}})} [\Delta_{\text{mix}}H_{\text{m}(\text{AC})}]_{x_{\text{A}(\text{AC})} = x_{\text{A}} + x_{\text{B}}/2}$$

$$+ \frac{4x_{\text{A}}x_{\text{B}}}{(2x_{\text{A}} + x_{\text{C}})(2x_{\text{B}} + x_{\text{C}})} [\Delta_{\text{mix}}H_{\text{m}(\text{AB})}]_{x_{\text{A}(\text{AB})} = x_{\text{A}} + x_{\text{C}}/2}$$

TABLE 2

Experimental values of the enthalpy of formation of the Cd–Ga–Sn liquid alloys (at 740 K) obtained by additions of tin to liquid binary Cd–Ga alloys ( $x_{\text{Cd}}/x_{\text{Ga}} = 1/3, 1/1$  and  $3/1$ ) and referred to the liquid state

| $x_{\text{Cd}}/x_{\text{Ga}} = 1/3$ |   | $x_{\text{Cd}}/x_{\text{Ga}} = 1/1$ |   | $x_{\text{Cd}}/x_{\text{Ga}} = 3/1$ |   |
|-------------------------------------|---|-------------------------------------|---|-------------------------------------|---|
| $x_{\text{Sn}}$                     | $\Delta_{\text{mix}}H_{\text{m}}$<br>(J mol <sup>-1</sup> ) | $x_{\text{Sn}}$                     | $\Delta_{\text{mix}}H_{\text{m}}$<br>(J mol <sup>-1</sup> ) | $x_{\text{Sn}}$                     | $\Delta_{\text{mix}}H_{\text{m}}$<br>(J mol <sup>-1</sup> ) |
| 0.0000                              | 2089  | 0.0000                              | 2598  | 0.0000                              | 2192  |
| 0.0598                              | 2159  | 0.0529                              | 2604  | 0.0570                              | 2366  |
| 0.0624                              | 2185  | 0.0649                              | 2598  | 0.0574                              | 2429  |
| 0.0732                              | 2212  | 0.0824                              | 2619  | 0.0789                              | 2397  |
| 0.1060                              | 2270  | 0.0997                              | 2626  | 0.0859                              | 2438  |
| 0.1187                              | 2169  | 0.1066                              | 2576  | 0.1043                              | 2457  |
| 0.1287                              | 2130  | 0.1175                              | 2531  | 0.1266                              | 2464  |
| 0.1481                              | 2201  | 0.1608                              | 2526  | 0.1758                              | 2443  |
| 0.1916                              | 2138  | 0.1678                              | 2494  | 0.2038                              | 2421  |
| 0.2047                              | 2115  | 0.1722                              | 2543  | 0.2282                              | 2390  |
| 0.2082                              | 2232  | 0.1765                              | 2561  | 0.2619                              | 2382  |
| 0.2124                              | 2162  | 0.2101                              | 2472  | 0.2734                              | 2377  |
| 0.2344                              | 2121  | 0.2305                              | 2441  | 0.2820                              | 2355  |
| 0.2591                              | 2097  | 0.2343                              | 2435  | 0.3272                              | 2294  |
| 0.2709                              | 2035  | 0.2542                              | 2397  | 0.3390                              | 2309  |
| 0.2858                              | 2064  | 0.2724                              | 2415  | 0.3419                              | 2231  |
| 0.2915                              | 2095  | 0.2962                              | 2295  | 0.3541                              | 2257  |
| 0.3061                              | 2026  | 0.3017                              | 2309  | 0.3809                              | 2181  |
| 0.3392                              | 1969  | 0.3102                              | 2296  | 0.3965                              | 2231  |
| 0.3640                              | 1950  | 0.3299                              | 2291  | 0.3987                              | 2192  |
| 0.3655                              | 1908  | 0.3385                              | 2211  | 0.4293                              | 2113  |
| 0.3711                              | 1974  | 0.3460                              | 2227  | 0.4347                              | 2067  |
| 0.3995                              | 1845  | 0.3759                              | 2209  | 0.4527                              | 2056  |
| 0.4043                              | 1929  | 0.3812                              | 2138  | 0.4578                              | 2109  |
| 0.4256                              | 1844  | 0.3906                              | 2152  | 0.4699                              | 2007  |
| 0.4374                              | 1791  | 0.4126                              | 2117  | 0.4907                              | 1956  |
| 0.4461                              | 1862  | 0.4304                              | 2035  | 0.5069                              | 1950  |
| 0.4504                              | 1794  | 0.4656                              | 1968  | 0.5199                              | 1896  |
| 0.4782                              | 1672  | 0.5121                              | 1876  | 0.5412                              | 1852  |
| 0.4823                              | 1706  | 0.5432                              | 1756  | 0.5530                              | 1823  |
| 0.4968                              | 1726  | 0.5758                              | 1644  | 0.5620                              | 1793  |
| 0.5002                              | 1691  |                                     |   | 0.5825                              | 1732  |
| 0.5135                              | 1573  |                                     |   |                                     |   |
| 0.5248                              | 1637  |                                     |   |                                     |   |
| 0.5276                              | 1626  |                                     |   |                                     |   |
| 0.5278                              | 1626  |                                     |   |                                     |   |
| 0.5343                              | 1569  |                                     |   |                                     |   |
| 0.5592                              | 1587  |                                     |   |                                     |   |
| 0.5678                              | 1507  |                                     |   |                                     |   |
| 0.5881                              | 1449  |                                     |   |                                     |   |
| 0.5901                              | 1432  |                                     |   |                                     |   |
| 0.6199                              | 1340  |                                     |   |                                     |   |

TABLE 3

Experimental values of the enthalpy of mixing at the intersection points (A, ..., I)

| Points | Sections                            | Coordinates  | $\Delta_{\text{mix}}H_{\text{m}}$<br>(J mol <sup>-1</sup> ) | $\Delta$<br>(%) |
|--------|-------------------------------------|--|---|-----------------|
| A      | $x_{\text{Cd}}/x_{\text{Ga}} = 1/3$ | $x_{\text{Cd}} = 0.0769$                             | 1117  | 0.01            |
|        | $x_{\text{Ga}}/x_{\text{Sn}} = 1/3$ | $x_{\text{Ga}} = 0.2308$<br>$x_{\text{Sn}} = 0.6923$ | 1115  |                 |
| B      | $x_{\text{Cd}}/x_{\text{Ga}} = 1/1$ | $x_{\text{Cd}} = 0.20$                               | 1570  | 0.8             |
|        | $x_{\text{Ga}}/x_{\text{Sn}} = 1/3$ | $x_{\text{Ga}} = 0.20$<br>$x_{\text{Sn}} = 0.60$     | 1596  |                 |
| C      | $x_{\text{Cd}}/x_{\text{Ga}} = 3/1$ | $x_{\text{Cd}} = 0.4286$                             | 2132  | 0.07            |
|        | $x_{\text{Ga}}/x_{\text{Sn}} = 1/3$ | $x_{\text{Ga}} = 0.1428$<br>$x_{\text{Sn}} = 0.4286$ | 2135  |                 |
| D      | $x_{\text{Cd}}/x_{\text{Ga}} = 1/3$ | $x_{\text{Cd}} = 0.1428$                             | 1839  | 0.03            |
|        | $x_{\text{Ga}}/x_{\text{Sn}} = 1/1$ | $x_{\text{Ga}} = 0.4286$<br>$x_{\text{Sn}} = 0.4286$ | 1718  |                 |
| E      | $x_{\text{Cd}}/x_{\text{Ga}} = 1/1$ | $x_{\text{Cd}} = 0.33$                               | 2270  | 3.4             |
|        | $x_{\text{Ga}}/x_{\text{Sn}} = 1/1$ | $x_{\text{Ga}} = 0.33$<br>$x_{\text{Sn}} = 0.33$     | 2432  |                 |
| F      | $x_{\text{Cd}}/x_{\text{Ga}} = 1/1$ | $x_{\text{Cd}} = 0.60$                               | 2428  | 2.0             |
|        | $x_{\text{Ga}}/x_{\text{Sn}} = 1/1$ | $x_{\text{Ga}} = 0.20$<br>$x_{\text{Sn}} = 0.20$     | 2528  |                 |
| G      | $x_{\text{Cd}}/x_{\text{Ga}} = 1/3$ | $x_{\text{Cd}} = 0.20$                               | 2153  | 0.12            |
|        | $x_{\text{Ga}}/x_{\text{Sn}} = 3/1$ | $x_{\text{Ga}} = 0.60$<br>$x_{\text{Sn}} = 0.20$     | 2148  |                 |
| H      | $x_{\text{Cd}}/x_{\text{Ga}} = 1/1$ | $x_{\text{Cd}} = 0.4286$                             | 2544  | 4.3             |
|        | $x_{\text{Ga}}/x_{\text{Sn}} = 3/1$ | $x_{\text{Ga}} = 0.4286$<br>$x_{\text{Sn}} = 0.1428$ | 2775  |                 |
| I      | $x_{\text{Cd}}/x_{\text{Ga}} = 3/1$ | $x_{\text{Cd}} = 0.6923$                             | 2356  | 3.0             |
|        | $x_{\text{Ga}}/x_{\text{Sn}} = 3/1$ | $x_{\text{Ga}} = 0.2308$<br>$x_{\text{Sn}} = 0.0769$ | 2428  |                 |

TABLE 4

Limiting molar partial enthalpies of cadmium and tin in binary and ternary alloys

| $\Delta H_{\text{m}\infty\text{Sn}}$<br>(J mol <sup>-1</sup> ) | Alloy   | $\Delta H_{\text{m}\infty\text{Cd}}$<br>(J mol <sup>-1</sup> ) | Alloy   |
|--|---|--|---|
| 3200 <sup>a</sup>  | Ga  | 6600 <sup>b</sup>  | Sn  |
| 5100   | Cd-Ga ( $x_{\text{Cd}}/x_{\text{Ga}} = 1/3$ ) | 7900   | Ga-Sn ( $x_{\text{Ga}}/x_{\text{Sn}} = 1/3$ ) |
| 5600   | Cd-Ga ( $x_{\text{Cd}}/x_{\text{Ga}} = 1/1$ ) | 9700   | Ga-Sn ( $x_{\text{Ga}}/x_{\text{Sn}} = 1/1$ ) |
| 7200   | Cd-Ga ( $x_{\text{Cd}}/x_{\text{Ga}} = 3/1$ ) | 10800  | Ga-Sn ( $x_{\text{Ga}}/x_{\text{Sn}} = 3/1$ ) |
| 9400 <sup>b</sup>  | Cd  | 12900 <sup>b</sup>   | Ga  |

<sup>a</sup>From ref. 19.<sup>b</sup>From ref. 11.



TABLE 5

Parameters obtained from the enthalpy data of the limiting binary systems and used in the Hoch–Arpshofen calculation

| System | $n(x)$ | $W$<br>(kK) | $W$<br>(J mol) | $\pm$<br>(kK) |
|--------|--------|-------------|----------------|---------------|
| Ga–Sn  | 2(Ga)  | 0.2097      | 1743.6         | 0.0024        |
| Ga–Cd  | 2(Ga)  | 0.6693      | 5564.0         | 0.0000        |
| Sn–Cd  | 3(Cd)  | 0.2031      | 1688.4         | 0.0027        |

The Hoch–Arpshofen model was derived originally by looking at associates in the solution and at the strength of the bond between atoms A and B which depends on the presence of the other atoms in the associate. This model was applied to binary, ternary and larger metallic systems [26, 27].

For a binary system AB, the enthalpy of mixing is represented by the following relation:

$$\Delta_{\text{mix}}H_{\text{m}} = Wnx(1 - x^{n-1})$$

where  $W$  is the interaction parameter,  $n$  is an integer (2, 3, 4, ...) and  $x$  is the molar fraction of the component so that the extremum of  $\Delta_{\text{mix}}H_{\text{m}}$  is at  $x > 0.5$ . The value of  $n$  is chosen such that  $W$ , determined from thermodynamic data, is independent of composition. From each experimental point, one value is obtained; all these can be averaged and a standard deviation obtained.

For a multicomponent system, the enthalpy of mixing is calculated from the enthalpy of binary systems using the general relation with  $x = x_i$ ,  $y = x_j$ , in the multicomponent system

$$\Delta_{\text{mix}}H_{\text{m}} = \sum_{ij} W_{ij} n_{ij} x [1 - (1 - y)^{n_{ij}-1}]$$

In Table 5 are collected the values of  $W$  and of  $n$  derived from experimental binary enthalpy data given by eqns. (1)–(3). For example the notation 2 (Ga) (Ga–Cd system) indicates that, in this system,  $n=2$  and  $x$  is the molar fraction of gallium to which the average value of  $W$  is equal to 0.6693 kK; the corresponding standard deviation is indicated in the column headed  $\pm$ .

In Figs. 2 and 3 the experimental and calculated values are reported. The discrepancies between the calculated enthalpies are small and of the same order of magnitude as the experimental error. Nevertheless the relation of Muggianu *et al.* has been retained and a correction term  $x_A x_B x_C (ax_A + bx_B + cx_C)$  has been introduced. The values of the coefficients  $a$ ,  $b$  and  $c$  are respectively  $-4.50(8) \text{ kJ mol}^{-1}$ ,  $+11.67(9) \text{ kJ mol}^{-1}$  and  $-4.59(3) \text{ kJ mol}^{-1}$  with  $x_A = x_{\text{Cd}}$ ,  $x_B = x_{\text{Ga}}$ ,  $x_C = x_{\text{Sn}}$ .

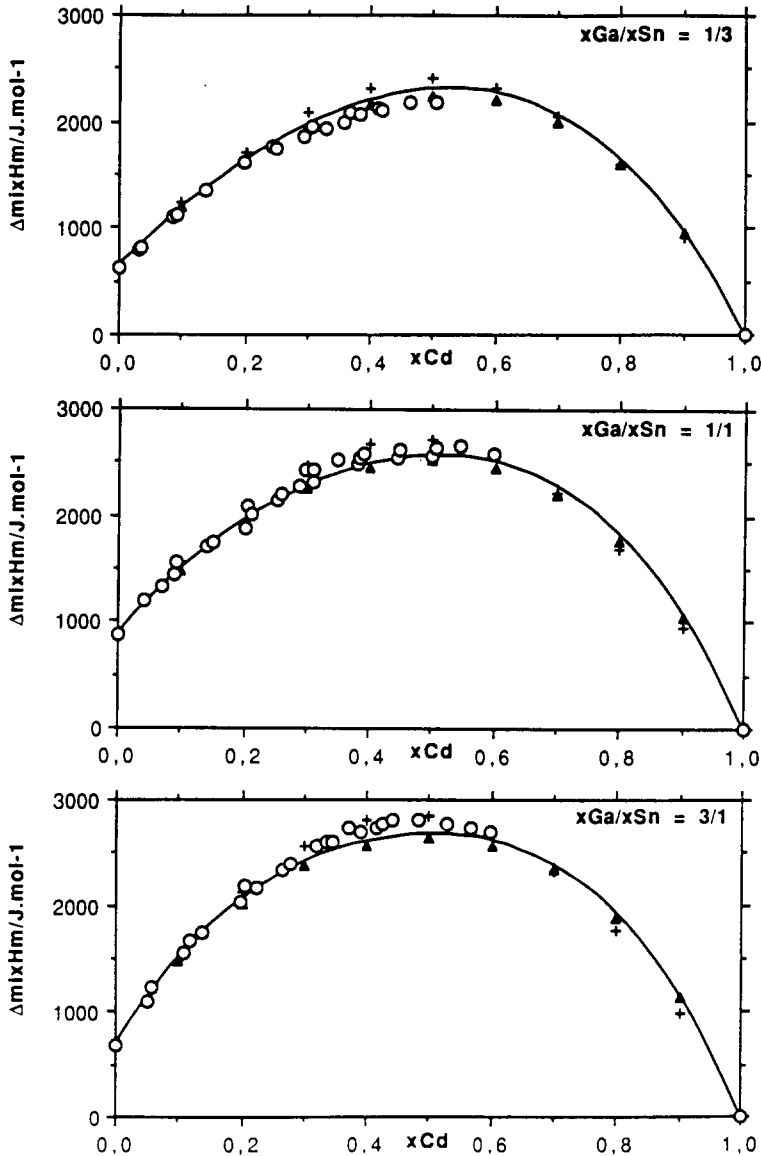


Fig. 2. Enthalpies of formation of Cd–Ga–Sn liquid alloys obtained by additions of solid cadmium to liquid Ga–Sn alloys at 740 K with  $x_{\text{Ga}}/x_{\text{Sn}} = 1/3$ ,  $1/1$  and  $3/1$ :  $\circ$ , experimental results; —, from the relation of Kohler;  $\blacktriangle$ , from the relation of Muggianu *et al.*; +, from the Hoch–Arpschhofen model.

## 5. Conclusion

The enthalpy of formation of the Cd–Ga–Sn liquid alloy has been measured by direct high temperature calorimetry and calculated from the corresponding enthalpy of formation of Cd–Ga, Cd–Sn and Ga–Sn systems already published

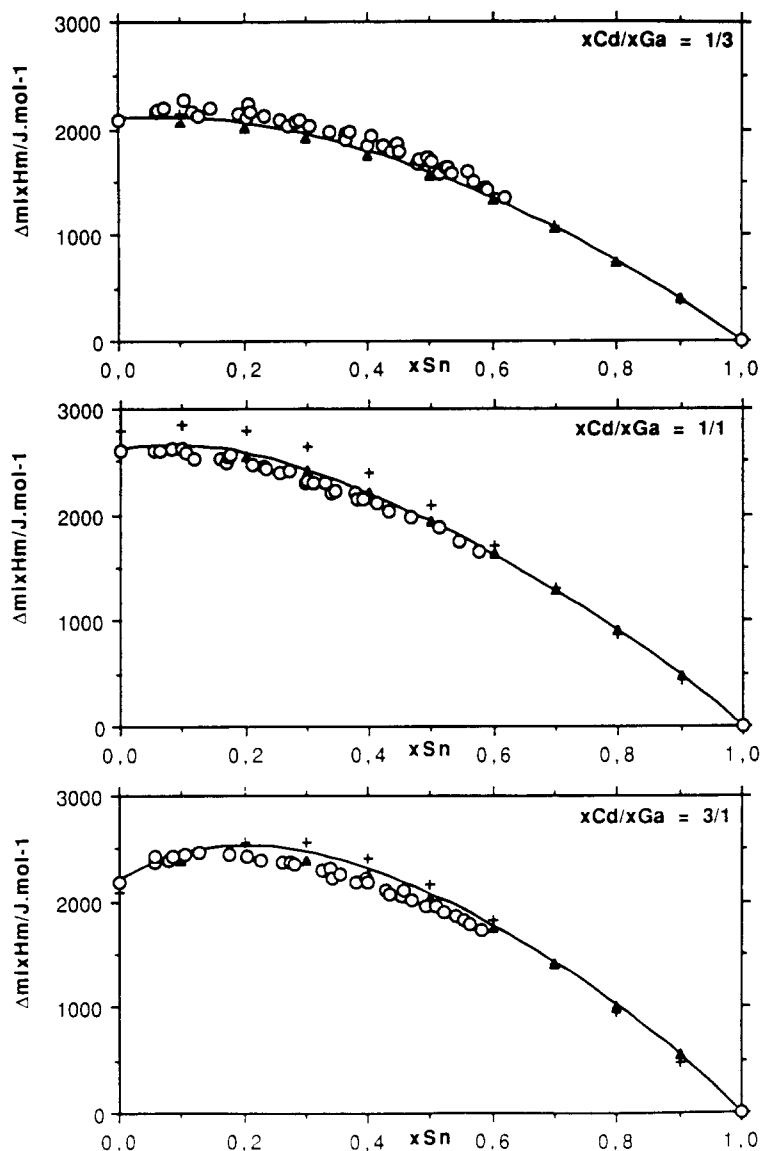


Fig. 3. Enthalpies of formation of Cd–Ga–Sn liquid alloys obtained by additions of solid tin to liquid Ga–Cd alloys at 740 K with  $x_{\text{Cd}}/x_{\text{Ga}} = 1/3$ ,  $1/1$  and  $3/1$ :  $\circ$ , experimental results; —, from the relation of Kohler;  $\blacktriangle$ , from the relation of Muggianu *et al.*; +, from the Hoch–Arpschhofen model.

using the Hoch–Arpschhofen model and two polynomial relations (due to Kohler and Muggianu *et al.*). The discrepancy between the calculated and experimental values is of the same order of magnitude as the experimental error. So, to represent the mixing enthalpy of Cd–Ga–Sn liquid alloy, over the entire

molar fraction range, the relation of Muggianu *et al.* with a ternary interaction term has been retained.

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